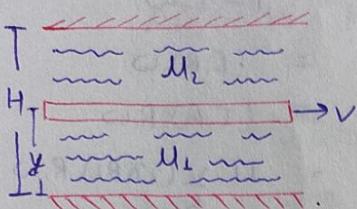


Nature ②

Pb - ③ gmp



$H \Rightarrow$ very small

a) $F_{D_1} = F_{D_2}$

$$\tau_1 A_1 = \tau_2 A_2 \quad (A_1 = A_2 = A)$$

$$\tau_1 = \tau_2$$

$$\mu_1 \frac{V}{y} = \mu_2 \frac{V}{(H-y)}$$

$$\mu_1(H-y) = \mu_2 y$$

$$\boxed{\frac{\mu_1 H}{(\mu_1 + \mu_2)} = y}$$

Determine y

- a) the drag force is equal on both sides of the plate
 b) the total drag force is mini.

I ES
To mark

b) $F_{DT} = F_{D_1} + F_{D_2}$

$$= \tau_1 A + \tau_2 A$$

$$= \mu_1 \frac{V}{y} A + \mu_2 \frac{V}{(H-y)} A$$

$$= V \cdot A \left(\frac{\mu_1}{y} + \frac{\mu_2}{(H-y)} \right)$$

For mini.

$$\frac{dF_{DT}}{dy} = 0$$

$$\sqrt{\frac{\mu_2}{H-y}} = \sqrt{\frac{\mu_1}{y}}$$

$$-\frac{\mu_1}{y^2} + \frac{\mu_2}{(H-y)^2} = 0$$

$$\boxed{y = \frac{H \cdot \sqrt{\mu_1}}{\sqrt{\mu_1} + \sqrt{\mu_2}}}$$

(Weight = Resistive force)

Mg = Resistive force

$$5 \times 9.81 = \tau \cdot A$$

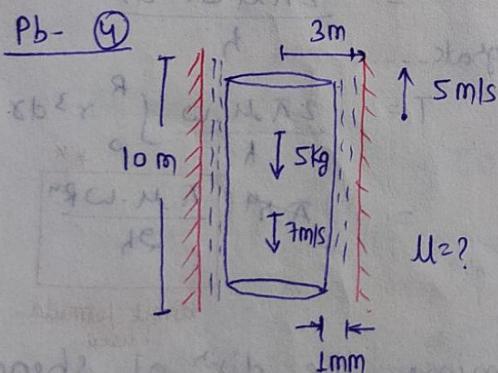
$$= \mu \cdot \frac{V}{h} \cdot A \quad (2\pi RL)$$

$$= \frac{\mu \times (7 - (-5)) \cdot (2\pi \cdot (3) \times 10)}{1 \times 10^{-3}}$$

$$\boxed{\mu = 2.16 \times 10^{-5} \frac{N \cdot s}{m^2}}$$

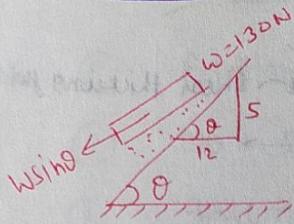
$$\boxed{\text{exert surface area of cylinder} = 2\pi r h + 2\pi r^2 \\ = 2\pi r(r+h)}$$

$$\boxed{\text{lateral surface area of cylinder} = (2\pi r h)}$$



$$\tau = \mu \frac{V}{h} \rightarrow \text{Relative velocity}$$

Pb-17



$$W \sin \theta = T_0 \cdot A$$

$$130 \times \frac{5}{13} = \mu \cdot \frac{V}{L} \cdot A = \mu \times 0.5 \times 1 =$$

$$\mu = 0.5 \text{ Ns/m}^2 \text{ Ans}$$

Rheology -

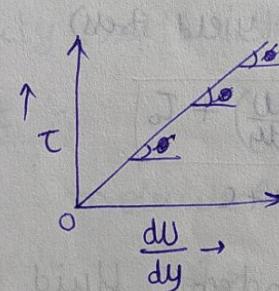
It is branch of science which deals with study of different type of fluid flow

Newtonian fluid :-

Obey's newton law

$$\tau = \mu \frac{du}{dy}$$

$$\gamma = M \cdot x$$



$$\text{slope of } \text{work} = \mu$$

example → oil, Kerosene, water, mercury, air, petrol

Non-Newtonian fluid :-

Don't obey newtonian fluid

$$\tau = A \left(\frac{du}{dy} \right)^n$$

A = consistency index

n = flow behaviour index

Pseudo-plastic

$$n < 1$$

$$\tau = A \cdot \left(\frac{du}{dy} \right)^n$$

$$\tau = \underbrace{A \cdot \left(\frac{du}{dy} \right)^{n-1}}_{\text{Apparent } \downarrow} \cdot \frac{du}{dy}$$

Apparent \downarrow

E.x. Blood
milk

Thixotropic

$$n > 1$$

$$\tau = A \cdot \left(\frac{du}{dy} \right)^n$$

$$\tau = \underbrace{A \cdot \left(\frac{du}{dy} \right)^{n-1}}_{\text{Apparent } \uparrow} \cdot \frac{du}{dy}$$

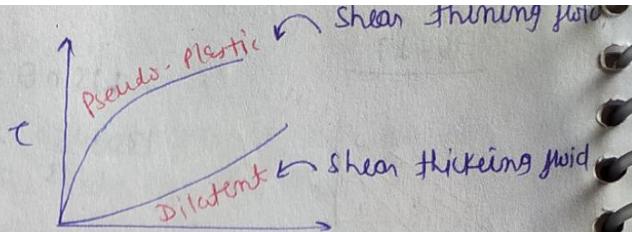
Apparent \uparrow

E.x. Saturated solution of sugar, Rice, starch, Honey.

Pseudo-plastic and

Dilatant are

"time independent fluid"



Bingham Plastic fluid :- [ideal Plastic] $\frac{dU}{dy}$

$$\tau = A \left(\frac{dU}{dy} \right)^n + B$$

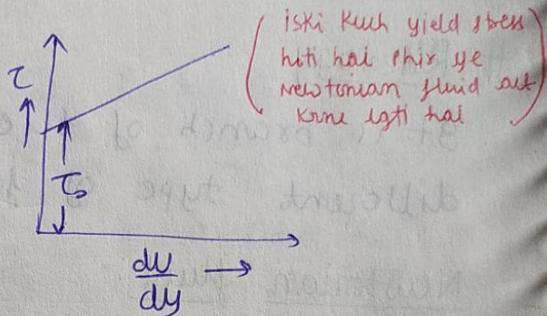
$$A = \mu$$

$$n = 1$$

$$B = \tau_0 \text{ (yield stress)}$$

$$\boxed{\tau = \mu \left(\frac{dU}{dy} \right) + \tau_0}$$

$$Y = mx + c$$



- Ex. - Toothpaste
- sewage sludge
- mud clay

time dependent fluid

$$\tau = A \left(\frac{dU}{dy} \right)^n + B$$

$$\downarrow \qquad \qquad \qquad \downarrow \qquad \qquad \qquad B > 0$$

Thixotropic
($n < 1$)

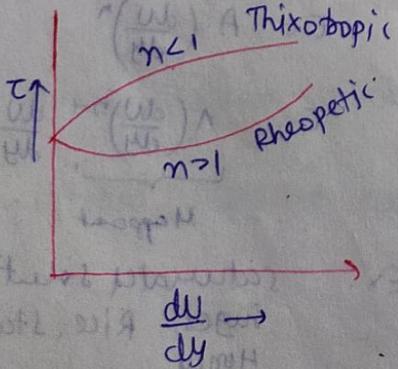
(M_{app} decreases
W.R.T time)

Ex: some paint
Poster inks

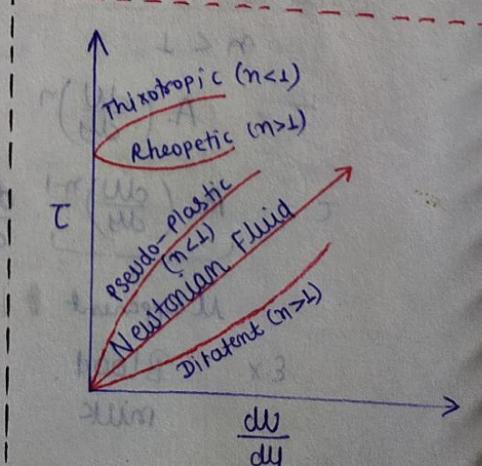
Rheopetic
($n > 1$)

(M_{app} increases
W.R.T time)

Ex: gypsum paste in water.

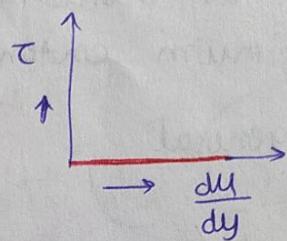


shear (const)
time



Ideal fluid :-

- ① Frictionless and "Inviscid fluid" ($\mu=0$) ($\tau=0$)
- ② No - surface tension.
- ③ Incompressible ④ viscosity zero



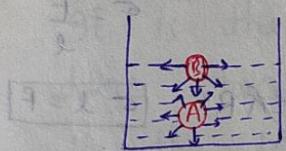
Visco-elastic fluid :-

these type of fluid having

- a properties of elasticity upto certain extent

Surface tension effect :-

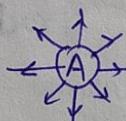
Experimental view



$$\sigma = 0.073 \text{ N/m}$$

for air & water
interface at
temp 0 20°C

molecule A (inside of liquid)

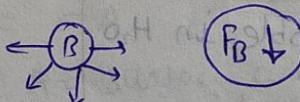


$$F_A = 0$$

$$\sigma = 0.480 \text{ N/m}$$

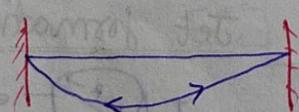
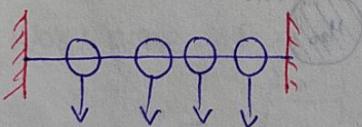
for air & mercury
interface at
temp 20°C

molecule B (At the surface)



$$F_B \downarrow$$

in general



in general

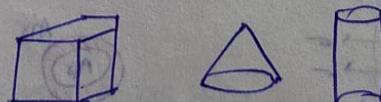
Volume fix

Maths →

$$\sigma = \frac{F}{L}$$

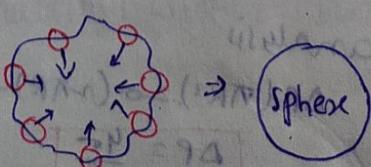
(F = tensile force)
(L = length)

i.e. = (the effect of cohesive
force at the surface)



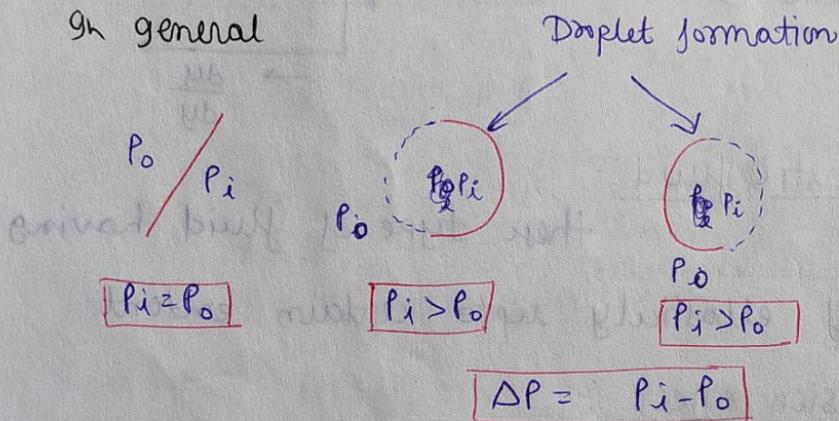
Sphere

(mini surface)
Area



It is the property of liquid by virtue of which tries to minimise the surface area upto the maximum extent.

In general



Water droplet →

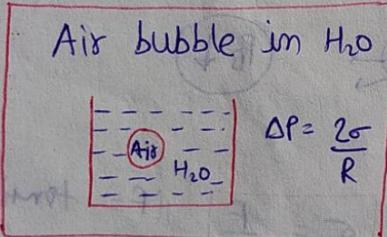
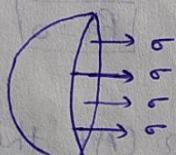
$$\text{Radius} = R \quad [\text{Pressure} = \frac{\text{Force} \times \text{Area}}{\text{Area}}]$$

Force analysis

$$\Delta P \cdot (\pi R^2) = \sigma (2\pi R) \quad [\sigma \cdot l = F]$$

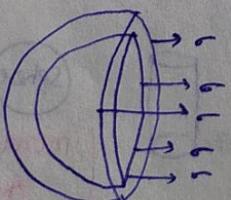
$$\Delta P = \frac{2\sigma}{R}$$

$$P = F \times A$$

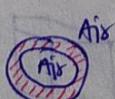


(Create special grp)

② Soap bubble :-



Radius = R

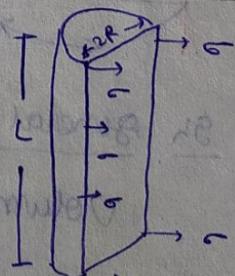


Force analysis

$$\Delta P \cdot (\pi R^2) = \sigma (2\pi R) + \sigma (2\pi R)$$

$$\Delta P = \frac{4\sigma}{R}$$

③ Jet formation



Force analysis

$$\Delta P (2R.L) = \sigma L + \sigma L$$

$$\Delta P = \frac{2\sigma}{R}$$