

Lecture ⑧
03/04/19

$$\left[\frac{\partial p}{\partial t} + \frac{\partial (pU)}{\partial x} + \frac{\partial (pV)}{\partial y} + \frac{\partial (pW)}{\partial z} = 0 \right]$$

Assumption →

① 3D-steady flow $\frac{\partial p}{\partial t} = 0$

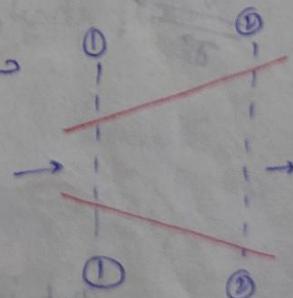
$$\frac{\partial (pU)}{\partial x} + \frac{\partial (pV)}{\partial y} + \frac{\partial (pW)}{\partial z} = 0$$

② 3D-steady incompressible flow ($\beta = \text{const}$)

$$\left(\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} + \frac{\partial W}{\partial z} \right) = 0$$

③ 2D-steady incompressible flow

$$\left(\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} \right) = 0$$



$$(\dot{m}_{in} - \dot{m}_{out})_x = \dot{m}_{storage}$$

$$\dot{m}_{in} - \left(\dot{m}_x + \frac{\partial \dot{m}_x}{\partial x} dx \right) = \frac{\partial \dot{m}}{\partial t} dv$$

(For steady flow)

$$-\frac{\partial \dot{m}}{\partial x} dx = 0$$

$\frac{\partial \dot{m}}{\partial x} = 0$, int it $\dot{m} = \text{constant}$

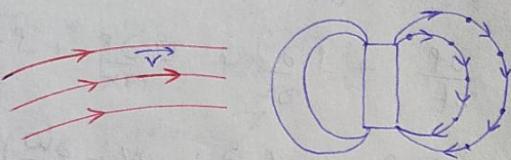
$\int A V = \text{constant}$

$$f_1 A_1 V_1 = f_2 A_2 V_2 \quad \text{if } f_1 = f_2$$

$$A_1 V_1 = A_2 V_2$$

Flow Representation:

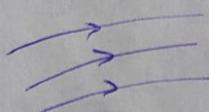
- Streamline
- Pathline
- Streakline



- ① S.L → Streamline is an imaginary curve drawn through a flowing field in such a way that a tangent to it at any point gives the dirn of the instantaneous velocity of flow at that point (instantaneous)
- ② These lines never cut each other in a flow

For steady flow

At $t=1, 2, 3$

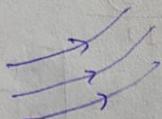


For unsteady flow

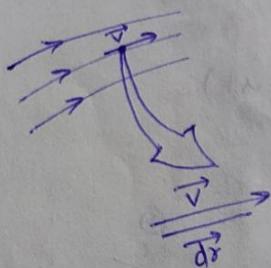
At $(t+\Delta t)$



At $t+\Delta t$



the eqn of streamline:



$$d\vec{s} = dx\hat{i} + dy\hat{j} + dz\hat{k}$$

$$\vec{V} = U\hat{i} + V\hat{j} + W\hat{k}$$

$$\vec{ds} \times \vec{V} = 0$$

$$\begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ dx & dy & dz \\ U & V & W \end{vmatrix} = 0$$

$$i(Wdy - Vdz) - j(Wdx - Udz) + k(Vdx - Udy) = 0$$

$$Wdy - Vdz = 0, \quad Wdx - Udz = 0 \quad \text{and}$$

$$Vdx - Udy = 0$$

$$\boxed{\frac{dx}{U} = \frac{dy}{V} = \frac{dz}{W}}$$

[Get it eqn of streamline]

- ① For 2D incompressible flow the velocity field is $2x\hat{i} - 2y\hat{j}$ determine the eqn of streamline passing from point (1,1)

$$\vec{V} = 2xi - 2y\hat{j}$$

streamline flow eqn

$$\frac{dx}{U} = \frac{dy}{V}$$

$$\frac{dx}{x} = -\frac{dy}{-xy}$$

$$\int \frac{dx}{x} = - \int \frac{dy}{y},$$

$$\log x = -\log(y) + \log(U)$$

$$\log x + \log(y) = \log U$$

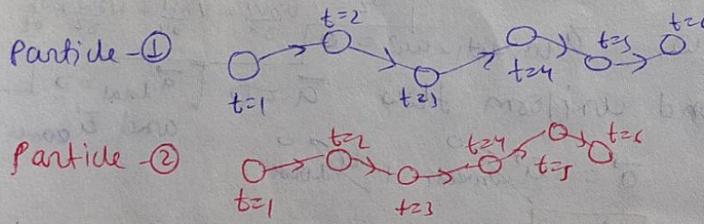
$$[xy = c]$$

$$\text{at } (1,1) \quad c=1$$

$$\text{then } \boxed{xy = 1}$$

Path line \rightarrow (lagrangian approach)

- ① It represent the actual path travelled by a fluid particle over a period of time
- ② These lines make cut one another



- ③ Streamline \rightarrow It is locus of fluid particle at a distance of which have cross through the same point

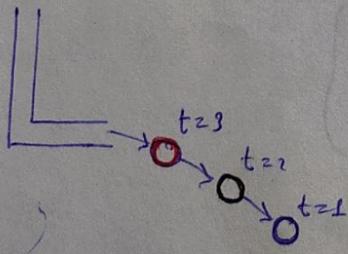
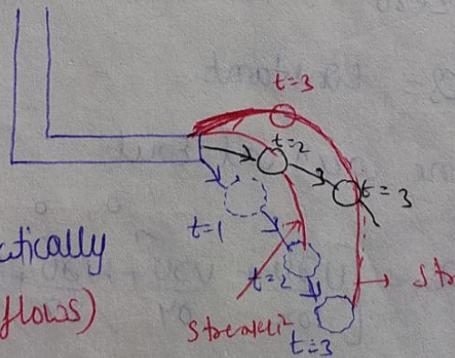
For unsteady flow:

\circ \rightarrow Particle - I

\circ \rightarrow Particle - 2

\circ \rightarrow Particle - ③

Note In physical, all the lines are different but mathematically they may be same (steady flows)



Streamline = dish of motion
(velocity)

Pathline = motion of a particular fluid particle

Streak line identification of location of different fluid

Particle

Acceleration

\vec{a} vector quantity

$$\vec{a} = a_x \hat{i} + a_y \hat{j} + a_z \hat{k} \quad |\vec{a}| = \sqrt{a_x^2 + a_y^2 + a_z^2} \text{ units}$$

$$\vec{a} = \frac{d\vec{v}}{dt}$$

$$\vec{v} = f^n(x, y, z, t)$$

$$\vec{v} = U \hat{i} + V \hat{j} + W \hat{k}$$

$$\frac{\partial \vec{v}}{\partial t} = \frac{\partial \vec{v}}{\partial x} \cdot dx + \frac{\partial \vec{v}}{\partial y} \cdot dy + \frac{\partial \vec{v}}{\partial z} \cdot dz + \frac{\partial \vec{v}}{\partial t} \cdot dt$$

$$\frac{\partial \vec{v}}{\partial t} = \frac{\partial \vec{v}}{\partial x} \cdot \frac{dx}{dt} + \frac{\partial \vec{v}}{\partial y} \cdot \frac{dy}{dt} + \frac{\partial \vec{v}}{\partial z} \cdot \frac{dz}{dt} + \frac{\partial \vec{v}}{\partial t}$$

$$\vec{a} = U \frac{\partial \vec{v}}{\partial x} + V \frac{\partial \vec{v}}{\partial y} + W \frac{\partial \vec{v}}{\partial z} + \frac{\partial \vec{v}}{\partial t}$$

$$U \frac{\partial v}{\partial x} + V \frac{\partial v}{\partial y} + W \frac{\partial v}{\partial z} = \text{convective acceleration}$$

$$\frac{\partial \vec{v}}{\partial t} = \text{temporal / local accn}$$

Theory **

- ① For steady flow, $\vec{a}_{\text{local}} = 0$
- ② For uniform flow, $\vec{a}_{\text{convective accn}} = 0$
- ③ For steady and uniform flow $\vec{a} = 0$ [$\vec{a}_{\text{local}} = 0$ and $\vec{a}_{\text{convective accn}} = 0$]

$$\vec{a} = \vec{a}_{\text{convective}} + \vec{a}_{\text{local}}$$

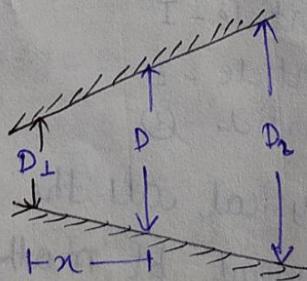
$$\boxed{\vec{a} = 0}$$

\Rightarrow in a fluid flow system where the velocity of net flow becomes zero is known as stagnation flow.

Pb - 18 $\rho = \text{constant}$

Determine a_x at exit

$$S.O.I^n = a_x = \left[U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} + W \frac{\partial U}{\partial z} + \frac{\partial U}{\partial t} \right]$$



$$a_x = U \frac{\partial U}{\partial x} \quad \left\{ \begin{array}{l} U = \frac{\rho}{\frac{\pi}{4} D^2} \\ \end{array} \right.$$

$$a_m = \frac{Q}{\frac{\pi}{4} D^2} \cdot \frac{\partial}{\partial x} \cdot \frac{Q}{\frac{\pi}{4} D^2} = \frac{Q^2}{\frac{\pi^2}{16} \times D^2} \cdot \frac{\partial}{\partial x} \left(\frac{1}{D} \right)$$

(by geometry) $a_m = \frac{D_2 - D_1}{L} = \frac{D - P_1}{B}$ $D = D_1 + B \cdot x$

\downarrow
B (assumed)

$$a_m = \frac{16}{\pi^2} \frac{Q^2}{(D_1 + B \cdot x)^2} \frac{\partial}{\partial x} \frac{1}{(D_1 + B \cdot x)^2}$$

$$a_m = \frac{16}{\pi^2} \frac{Q^2}{(D_1 + B \cdot x)^2} \times \frac{(-2)}{(D_1 + B \cdot x)^2} \times B$$

$$a_m = \frac{-32 Q^2 (D_2 - P_1)}{\pi^2 (D_1 + B \cdot x)^5 \cdot L}$$

At exit $x = L$

$$a_m = \frac{-32 Q^2 (D_1 - D_1)}{\pi^2 (D_1 + L \cdot B)^5 \cdot L} = \frac{-32 Q^2 (P_2 - P_1)}{\pi^2 \times (D_1 + L \cdot B)^5 \cdot L}$$

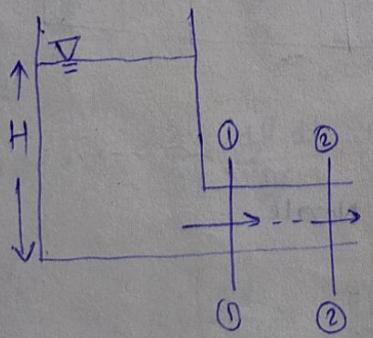
$$a_m = \frac{-32 Q^2 (D_2 - D_1)}{\pi^2 \cdot B \times (D_1 + D_2 - D_1)^5 \cdot L} = \frac{-32 Q^2 (D_2 - D_1)}{\pi \cdot L \cdot L \cdot (D_2)^5 \cdot B}$$

$$c_m = \frac{-32 Q^2 (x_2 - x_1)^2}{\pi^2 \cdot B \cdot (x_2)^5 \cdot L \times 8} = \frac{32 Q^2 (x_1 - x_2)^2}{\pi^2 \cdot L \cdot (x_2)^5 \times 8}$$

$$a_m = \frac{2 g_2 (x_1 - x_2)^2}{\pi^2 \cdot L \cdot (x_2)^5 \cdot B} = \boxed{\frac{2 g_2 (x_1 - x_2)^2}{\pi^2 \cdot L \cdot R_2^5}}$$

$$\frac{\left(\frac{m^3}{s}\right)^2 (m)}{m \cdot m^2} \Rightarrow \frac{m}{s^2}$$

Case - I



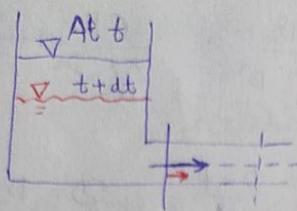
$$(V_1 = V_2)$$

$$(A_1 = A_2)$$

$$\vec{a} = \vec{a}_{\text{geometric}} + \vec{a}_{\text{local}}$$

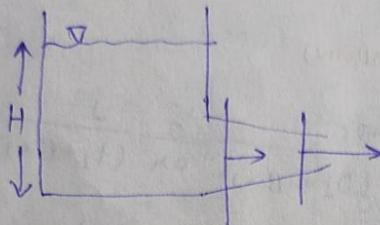
$$\boxed{\vec{a} = 0}$$

Case - ②



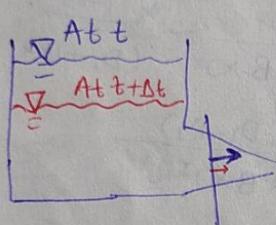
$$\vec{a} = \vec{a}_{\text{conv}}^{\circ} + \vec{a}_{\text{local}}$$

Case - ③



$$\vec{a} = \vec{a}_{\text{conv}}^{\circ} + \vec{a}_{\text{local}}$$

Case - ④



$$\vec{a} = \vec{a}_{\text{conv}}^{\circ} + \vec{a}_{\text{local}}$$

Motion on curved path :

a_t (Tangential $a_c(\gamma)$) \Rightarrow due to change in magnitude

a_N (Normal $a_c(\gamma)$) \Rightarrow due to change in direction

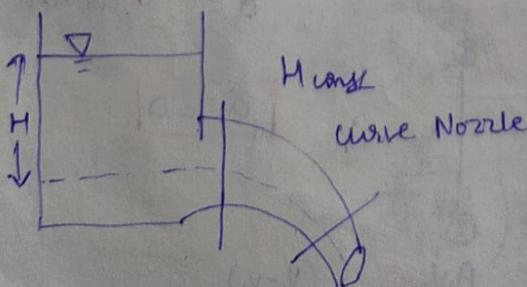
$$a_t = \frac{v^2}{r}$$

r = Radius of curvature

S.No.

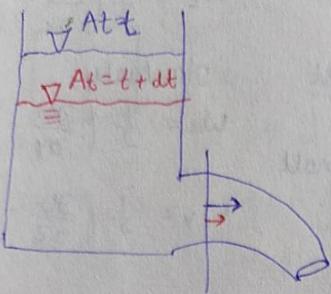
		H_{const}	H_{varying}
1	convective	$\cancel{H_{\text{const}}}$	$\cancel{H_{\text{varying}}}$
	Normal	\checkmark	\checkmark
2	Local	\times	\checkmark
	Normal	\times	\times

Case ⑤

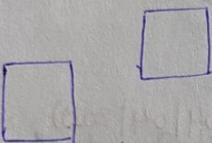


Case - ⑥

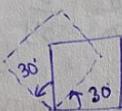
If dimensions remain constant then tangential velocity ω



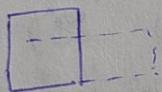
Rotational Parameters in flow \rightarrow



Translation



(Pure Rotation) $\left(\frac{30+30}{2}\right)$



linear deformation

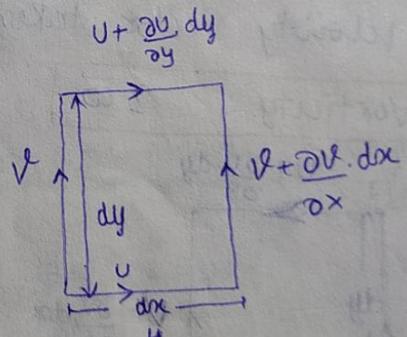


Shear deformation

angular velocity

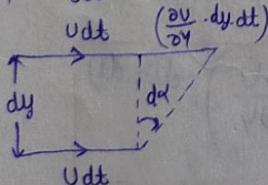
Angular Velocity (ω)

in $x-y$ plane $U + \frac{\partial U}{\partial Y} \cdot dy$



contribution of U -velocity in rotation :-

In dt time interval



$$\tan \delta \omega = -\frac{\partial U}{\partial Y} \cdot \frac{dy \cdot dt}{dx} \quad \left\{ \begin{array}{l} \text{dx} \Rightarrow \text{very small} \\ \tan \delta \approx \delta \end{array} \right.$$

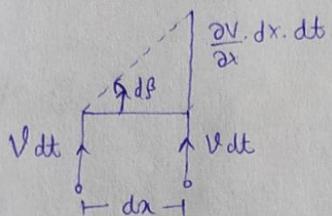
sign convention

\rightarrow clockwise
 \leftarrow Anticlockwise

$$\frac{d\omega}{dt} = -\frac{\partial U}{\partial Y}$$

Contribution of v-velocity in rotation →

In dt time interval -



$$\tan d\beta = \frac{\partial V}{\partial x} \cdot \frac{dx \cdot dt}{dx}$$

$\therefore d\beta = \text{very-2 small}$

$$\boxed{\frac{d\beta}{dt} = \frac{\partial V}{\partial x}}$$

$$\omega_z = \frac{1}{2} \left(\frac{\partial V}{\partial x} - \frac{\partial U}{\partial y} \right)$$

similarly,

$$\omega_x = \frac{1}{2} \left(\frac{\partial \omega}{\partial y} - \frac{\partial V}{\partial z} \right)$$

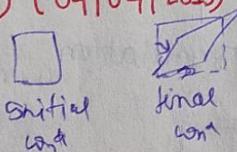
$$\omega_y = \frac{1}{2} \left(\frac{\partial U}{\partial z} - \frac{\partial \omega}{\partial x} \right)$$

$$\vec{\omega} = \omega_x \hat{i} + \omega_y \hat{j} + \omega_z \hat{k}$$

$$\vec{\omega} = \frac{1}{2} [\vec{\nabla} \times \vec{V}] = \frac{1}{2} \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \end{vmatrix} =$$

Rate of shear strain : (lecture 9) (04/04/2019)

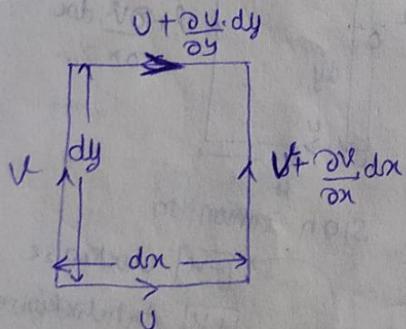
$$g_h \text{ in } x-y \text{ plane} = \frac{1}{2} \left[\frac{\partial V}{\partial x} + \frac{\partial U}{\partial y} \right]$$



circulation: (Γ) [Capital Gamma]

It is defined as the line integration of velocity vector taken along a close loop

Vorticity : $2 \vec{\omega}$



$$\Gamma = \oint \vec{V} \cdot d\vec{s}$$

in x-y Plane

$$\Gamma = U dx + \left(V + \frac{\partial V}{\partial x} dy \right) dy - \left(U + \frac{\partial U}{\partial y} dx \right) dx - (V dy)$$

$$\boxed{\Gamma = \left(\frac{\partial U}{\partial x} - \frac{\partial V}{\partial y} \right) dx dy}$$

Pb-②

$$U = 2u + 3y \quad \text{so h}$$

$$V = 2y$$

$$r = 2 \text{ units}$$

$$\Gamma = \left(\frac{\partial U}{\partial x} - \frac{\partial V}{\partial y} \right) dx dy$$

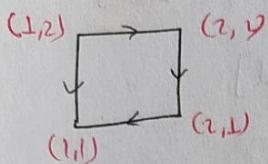
$$= (0 - 3)(\pi r^2)$$

$$= -3\pi \text{ (Ans)}$$

(Pb)

$$V = x^2$$

$$V = -2xy$$



$$\text{Sgn } \Gamma = \int_{n=1}^{x=2} V \cdot dx + \int_{y=1}^{y=2} (V \cdot dy) + \int_{x=2}^{x=1} (V \cdot dy) + \int_{y=2}^{y=1} (V \cdot dx)$$

$$\begin{aligned}
 &= \int_1^2 x^2 dx + \int_1^2 -2(y) y \cdot dy + \int_2^1 x^2 \cdot dy + \int_2^1 -2(1) y \cdot dy \\
 &= \int_1^2 x^2 dx - 4 \int_1^2 y \cdot dy + \int_2^1 x^2 \cdot dy - 2 \int_2^1 y \cdot dy \\
 &= -4 \left[\frac{y^2}{2} \right]_1^2 - 2 \left[\frac{y^2}{2} \right]_2^1 \\
 &= -\frac{4}{2} [4-1] - \frac{2}{2} [1-4] \\
 &= -2(3) - 1(-3) \\
 &= -6 + 3 = -3
 \end{aligned}$$

- velocity potential function (ϕ)
 → stream function (ψ)

(V.P.F) (ϕ) In general V.P.F is defined as a sum of space and time in a flow such that the negative derivative of this sum w.r.t any dist gives the velocity of fluid flow in that dist.

Boundary with ϕ , continuity eqn for 2D - steady, incompressible flow,

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0$$

$$\frac{\partial}{\partial n} \left(-\frac{\partial \phi}{\partial x} \right) + \frac{\partial}{\partial y} \left(-\frac{\partial \phi}{\partial y} \right) = 0$$

$$-\frac{\partial^2 \phi}{\partial x^2} - \frac{\partial^2 \phi}{\partial y^2} = 0$$

$$\frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} = 0$$

$$\rightarrow \boxed{\nabla^2 \phi = 0}$$

Laplace eqn

ϕ must satisfy Laplace eqn

(Pb)

$$\phi = 2x + 3y$$

$$\boxed{\nabla^2 \phi = 0}$$

ϕ = valid

irrotational flow

(ii)

$$\phi = 4x^2 - 5y^2$$

$$\nabla^2 \phi = 2$$

$\neq 0$

ϕ = invalid

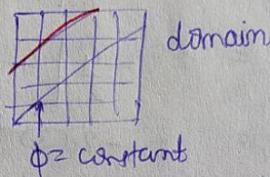
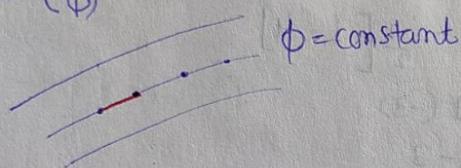
Physical significance

$$\omega_z = \frac{1}{2} \left[\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right] = \frac{1}{2} \left[\frac{\partial}{\partial x} \left(\frac{-\partial \phi}{\partial y} \right) - \frac{\partial}{\partial y} \left(-\frac{\partial \phi}{\partial x} \right) \right] = 0$$

[ϕ exist \rightarrow irrotational]

Equation of equipotential funⁿ line:

These line (curve) are formed by joining the different point adding having the same value of velocity potential funⁿ (ϕ)



$$\text{Ex: } 2x + 3y$$

for 2D steady incompressible flow

$$\phi = f(x, y)$$

$$d\phi = \frac{\partial \phi}{\partial x} dx + \frac{\partial \phi}{\partial y} dy = -U dx - V dy$$

$$0 = -U dx - V dy, \quad U dx + V dy = 0$$

$$\boxed{\left. \frac{dy}{dx} \right|_{\phi=\text{const}} = -\frac{U}{V}}$$

Stream funⁿ: (ψ) in general

it is a funⁿ of space and time in a 2D (x-y plane) define in such a way i.e. continuity eqn satisfy and flow is possible.

continuity eqn

For 2D - steady ; incompressible flow

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\left. \begin{aligned} \text{If } u &= -\frac{\partial \psi}{\partial y} \\ v &= \frac{\partial \psi}{\partial x} \end{aligned} \right\}$$

$$\text{then, } \frac{\partial}{\partial x} \left(-\frac{\partial \psi}{\partial y} \right) + \frac{\partial}{\partial y} \left(\frac{\partial \psi}{\partial x} \right) = 0 \quad (0=0)$$

continuity satisfied

check

$$\omega_z = \frac{1}{2} \left[\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right] = \frac{1}{2} \left[\frac{\partial}{\partial x} \left(\frac{\partial \psi}{\partial y} \right) - \frac{\partial}{\partial y} \left(-\frac{\partial \psi}{\partial x} \right) \right] = \frac{1}{2} \left[\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} \right]$$

$$= \frac{1}{2} |\nabla^2 \psi|$$

[If $\nabla^2 \psi = 0$, Irrotational flow]
 [If $\nabla^2 \psi \neq 0$, Rotational flow]

Pb- 34

$$\Psi = P_n x + q_n y$$

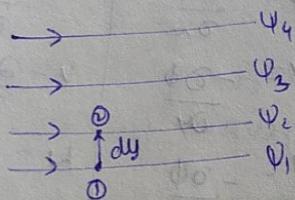
If ϕ exist means irrotational flow

$$\nabla^2 \phi = 0$$

$$2P + 2q = 0$$

$$\boxed{P = -q}$$

Physical significance :



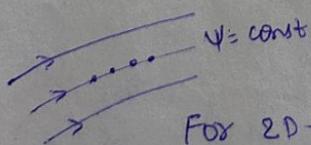
Assume width = 1

For 2D - steady incompressible flow

$$\Psi = f^n(x, y)$$

Math. $d\Psi = \left(\frac{\partial \Psi}{\partial x} \right) dx + \left(\frac{\partial \Psi}{\partial y} \right) dy$

Eqn of Equisetum funt line :- these lines (curves) are formed by joining the different points having the same value of stream function (Ψ).



For 2D - steady, incompressible flow,

$$\Psi = f^n(x, y)$$

Math. $d\Psi = \left(\frac{\partial \Psi}{\partial x} \right) dx + \left(\frac{\partial \Psi}{\partial y} \right) dy$

$$0 = U \cdot dx - U \cdot dy$$

$$d\Psi = -U (dy \perp)$$

$$-d\Psi = dQ \text{ per unit width}$$

Int it.

$$-\int_1^2 d\Psi = Q \text{ per unit width}$$

$$\boxed{\Psi_2 - \Psi_1 = Q \text{ per unit width}}$$

Pb 35 $\Psi_L = \frac{3}{2} (z - L)$

$$\Psi_2 = 0$$

$$|\Psi_1 - \Psi_2| = 12 \text{ units}$$

discharge (q.e)

$$U \, dy = V \, dx$$

$$\boxed{\frac{dx}{U} = \frac{dy}{V}}$$

$$\left. \frac{dy}{dx} \right|_{\psi \rightarrow \text{const.}} = \frac{V}{U}$$

Note: $\left. \frac{dy}{dx} \right|_{\Phi \rightarrow \text{const.}} \times \left. \frac{dy}{dx} \right|_{\psi \rightarrow \text{const.}} = -\frac{U}{V} \times \frac{V}{U} = -1$

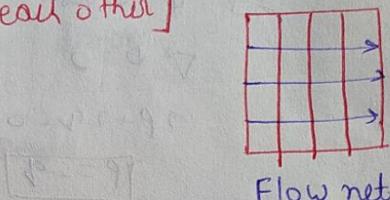
[Equi-potential lines and equi stream fun.
lies are orthogonal to each other]

Cauchy-Riemann eqn:

For irrotational flow

$$U = \boxed{-\frac{\partial \phi}{\partial x} = -\frac{\partial \Psi}{\partial y}}$$

$$V = \boxed{-\frac{\partial \phi}{\partial y} = +\frac{\partial \Psi}{\partial x}}$$



Flow net

$$\text{Sign } U = -\frac{\partial \phi}{\partial x}$$

$$V = -\frac{\partial \phi}{\partial y}$$

$$W = -\frac{\partial \phi}{\partial z}$$

$$U = \frac{\partial \phi}{\partial x}$$

$$V = \frac{\partial \phi}{\partial y}$$

$$W = \frac{\partial \phi}{\partial z}$$

Pb 48 For 2D Incompressible flow field

$$U = \frac{y^3}{3} + 2xy - x^2y$$

$$V = xy^2 - 2y - \frac{x^3}{3}$$

Soh For 2D incompressible flow

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} = 0$$

$$(2 - 2xy) + (2xy - 2) = 0$$

$$0 = 0$$

continuity satisfied

flow is possible

$$\left(\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} \right) = 0$$

$$\begin{aligned} U &= -\frac{\partial \Psi}{\partial y} & \text{anti} \\ V &= \frac{\partial \Psi}{\partial x} & \text{unity} \\ \text{eqn} & \end{aligned}$$

Obtain Ψ

$$-\frac{\partial \Psi}{\partial y} = U$$

$$\frac{\partial \Psi}{\partial y} = -\frac{y^3}{3} - 2xy + x^2y$$

$$\text{Gnt it } \Psi = -\frac{y^4}{12} - 2xy + \frac{x^2y^2}{2} + f(x) + \text{constant}$$

$$\frac{\partial \Psi}{\partial x} = v$$

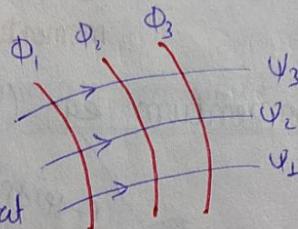
$$\frac{\partial \Psi}{\partial x} = 2xy - 2y - \frac{y^3}{3}$$

gnt it:

$$\Psi = \frac{x^2y^2}{2} - 2xy - \frac{y^4}{12} + f(y) + \text{const.}$$

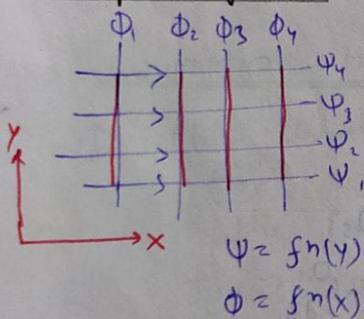
$$\boxed{\Psi = \frac{x^2y^2}{2} - 2xy - \frac{y^4}{12} - \frac{y^7}{12} + \text{const}}$$

Flow Net: for irrotational flow.

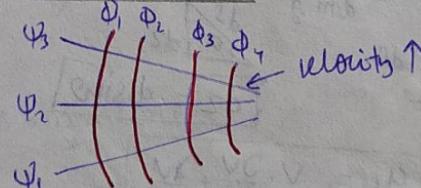


It is a graphical representation of equipotential and stream lines.

Uniform Flow →



Aux Flow:

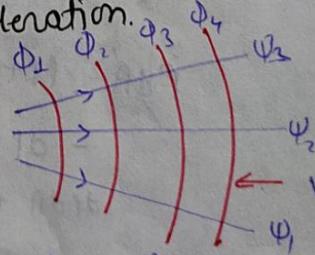


Exira

$$Q = \text{constant}$$

$$Q = A.V$$

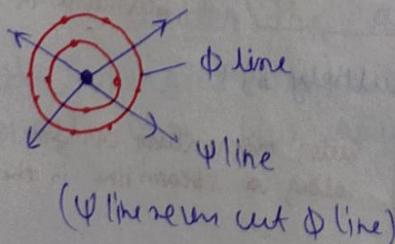
Deceleration



Sink
(radially inland)

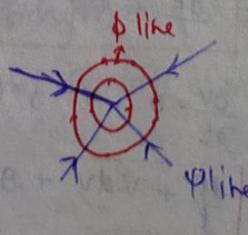
Source

(Radially outward)



$$\Psi = f_n(\theta)$$

$$\Phi = f_n(r_n\theta)$$



Fluid Dynamic (Chapter)

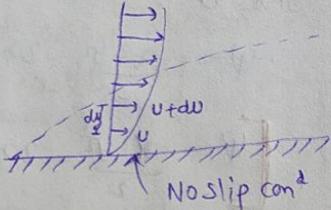
Study of motion of fluid with considering the basic cause of motion (External)

Flow over a flat plate:

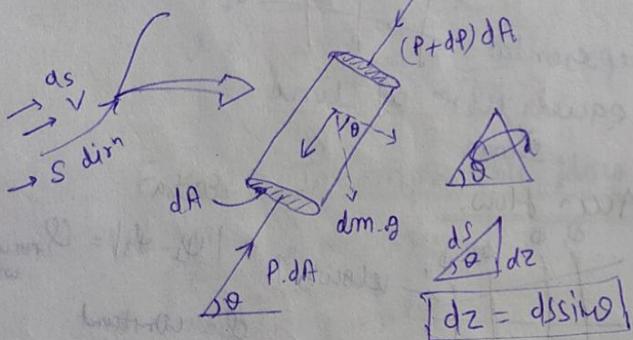
inviscid Region of fluid flow [$F_{vis} \approx 0$]

$$F_p + F_g = F_i \quad (\text{Euler momentum eqn})$$

$$F_p + F_g + F_{vis} = F_i \quad (\text{Navier's Stoke momentum eqn})$$



Euler momentum eqn (flow along stream line)



$$ds = V \cdot \frac{\partial V}{\partial S} + \frac{\partial V}{\partial t} \quad **$$

$$P.dA - (P+dp).dA - dm.g \sin\theta = dm.ds$$

$$- dp.dA - dm.g \sin\theta = dm.ds \quad 0$$

$$dp.dA + g(ds.dA) \left[V \frac{\partial V}{\partial S} + \frac{\partial V}{\partial t} \right] + g(ds) \left(dm \sin\theta \right) = 0$$

Divide by g

$$\frac{dp}{g} + ds \left[V \frac{\partial V}{\partial S} + \frac{\partial V}{\partial t} \right] + g dz = 0 \quad \text{Euler momentum eqn along a streamline in the direction of flow}$$

→ steady flow
 $\frac{\partial V}{\partial t} = 0$, $V = f^n(S, t)$ multiply by g

$$\frac{dp}{g} + V \cdot dV + g dz = 0$$

Euler momentum eqn for steady flow along a streamline in the flow direction

Int. it

$$\int \frac{dp}{g} + \frac{V^2}{2} + g z = \text{const}$$

Incompressible Flow $\rightarrow f \rightarrow \text{const}$

$$\frac{P}{f} + \frac{V^2}{2} + g.z = \text{constant}$$

$$P + \frac{1}{2} \rho V^2 + \rho g.z = \text{const}$$

Bernoulli's eqn